

# **Down Hole Flow Assurance**

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# **Flow Assurance Key Words**

- SCSSV Setting Depth
- SITP
- Scale
- Hydrate
- Wax
- Corrosion
- Asphaltene
- Chemical Injection
  - Methanol
  - Glycol
  - LDHI
  - Corrosion Inhibitor
  - Scale Inhibitor
- Gas Lift
- ESP
- Scale Squeeze

- h · Acid Job
  - Sand
  - Slugging
  - Erosion
  - JT Cooling/Heating
  - Water Hammer
  - VIT
  - Insulation
  - Proppant
  - Annulus Management
  - SCSSV Testing
  - Cooldown time
  - Warmup time
  - Maximum
    Temperature
  - Minimum Temperature

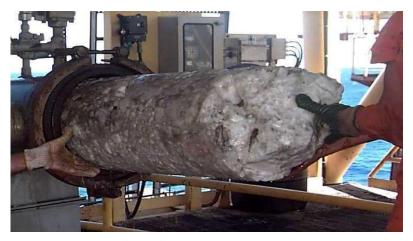


- OHTC
- Fluid & Material Compatibility
- C-Factor
- Multiphase Flow
  Correlations
- OLGA
- Fluid properties
- Geothermal
  Temperature Gradient
- Emulsion
- Souring
- Etc.

#### **Hydrates**

#### Hydrate Formation Locations

- Tubing
- Annulus
- Safety Valves
- Well Servicing Well Control Equipment
  - Wireline Lubricators
- Wellheads and Trees
- Chokes
- Chemical Injection Lines
- Outside of well

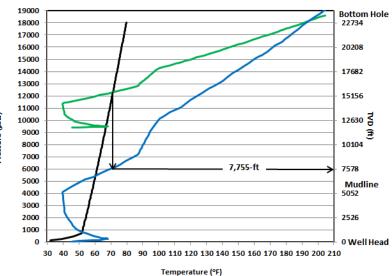


Petrobras



- Hydrate Risk Zone and SCSSV Setting Depth
  - Compare hydrate curve, SITP conditions and geothermal temperature gradient.
  - Determine hydrate formation temperature, pressure, and depth.
  - From geothermal temperature gradient, determine boundary depth for hydrate risk zone.
  - Consider effect of
    - Gas lift
    - ESP

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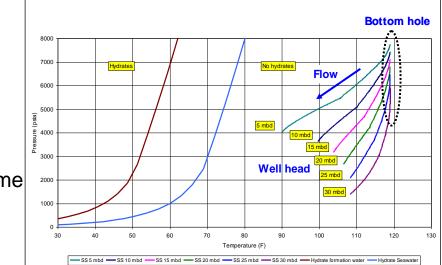
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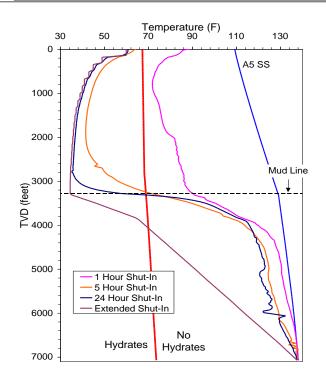
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CV

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SDV





#### Hydrate Management

- Shutdown Cooldown time
- Re-Start Warmup time
- Inhibitor Injection: rate, duration, volume
- Insulation
- Bullheading
- Depressurization
- Coiled Tubing



# Scale

- Precipitation and deposition of inorganic minerals within the production wells and processing equipment.
  - Depends on several of factors
    - Water Composition
    - pH
    - Pressure
    - Temperature
    - CO<sub>2</sub> Concentration
    - Compatibility of Waters
    - Chemicals Affecting Solubility Limits



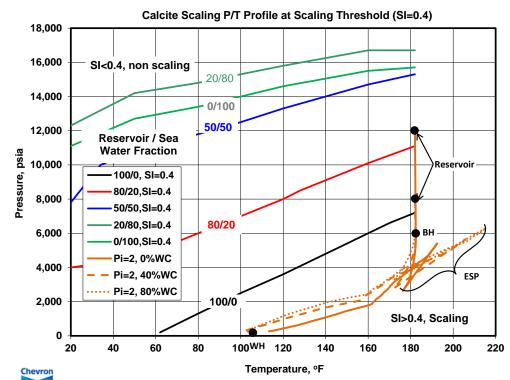
Nalco



#### Calcite Scaling

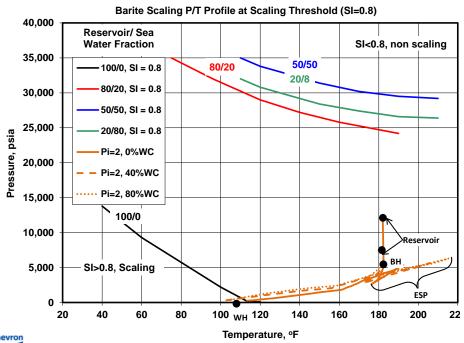
- Calcite scaling tendency increases with increasing temperature and decreasing pressure.
  - High up in the tubing due to lower pressures
  - Around ESP due to high temperature
  - At downhole flow restrictions (Perforations, nipples, etc.)
- Precipitation can occur as the pH of the brine increases. Unlike many salts, the solubility of CaCO<sub>3</sub> decreases at higher temperature
  - Resulting in precipitation in heat transfer equipment or ESP's

- Mixing incompatible waters can also increase carbonate scaling tendency.
- Carbonate Scales can develop low in the well, clogging downhole equipment, and plugging perforations.



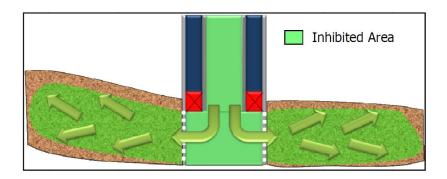
#### Barium Sulfate Scaling

- Barite scaling tendency increases with decreasing temperature or decreasing pressure with temperature having a greater effect.
  - It is generally a problem in the upper well bore or production facilities.
- Mixing sulfate-rich seawater with barium-rich formation water most common risk.
  - Seawater injection can lead to sulfate scaling in the reservoir due to water incompatibility
  - When seawater is used in a workover or completion operation, sulfate scales are also a risk then
  - When water flooding with seawater, there typically is a risk of Sulfate Scales
    - It is common to remove sulfate from seawater if it will be used for water flooding



### Scale Mitigation and Remediation

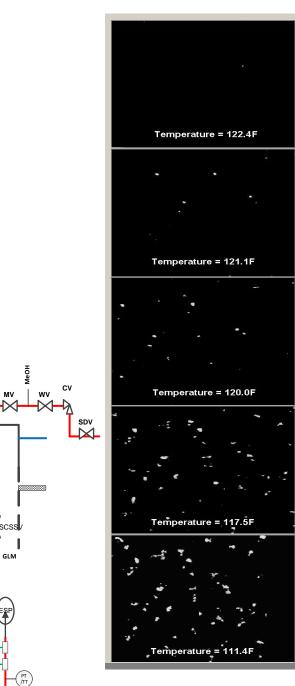
- Preemptive Scale Squeeze
- Down Hole Scale Inhibitor Injection
- Scale Squeeze
- Acid Injection
- Coiled Tubing





#### Wax Deposition

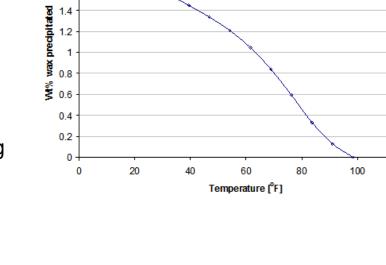
- Wax deposits in the upper portion of the wellbore, where the fluids have cooled below the cloud point or WAT.
  - WAT varies greatly in oils and condensates; it can range between 50 – 120°F
  - Pour point also varies depending of wax content. It \_ can range 20 - 80°F.
- Wax deposition is temperature driven.
  - Temperature Control Preventing hydrocarbons from cooling prevents wax from Wax Risk Zone depositing
  - Vacuum insulated tubing
  - Insulating packer fluid
  - Low risk during shutdowns
  - High risk operating at low rates and temperatures



SI MeOF Gas

#### Wax Management

- Wax Inhibitors and pour point depressants
  (PPD) injection
- Hot Oiling Hot Oil is circulated in the well, melting any wax in the well, allowing it to be flowed out
- Chemical Solvents Terpenes or Aromatic
  Solvents can be effective at wax removal
- Mechanical Removal Slick line operation to cut was deposition from the inside of the tubing combined with solvent soaking.
  - Frequency of wire line interventions
  - Well downtime during wax cutting
  - Risk of sticking wire line tools
- Coiled Tubing (to inject hot fluid or solvent)



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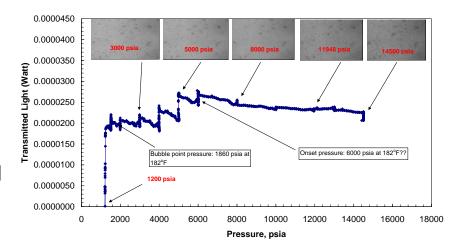
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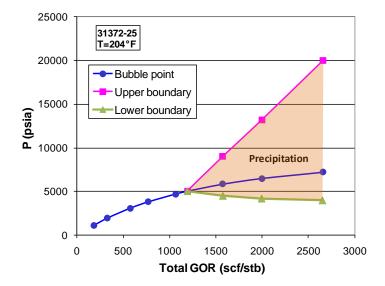


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# Asphaltenes

- Asphaltenes may precipitate when the fluid conditions change (particularly pressure) or incompatible fluid streams are mixed.
  - Transition across the bubble point results in a major change in density and thus a change in asphaltene stability
    - Further changes in pressure will result in changes in density
  - Mixing of heavy oil with lighter oil
  - Gas Lift
  - CO<sub>2</sub> Injection



















#### Asphaltene Management

- Asphaltene inhibitors can be injected downhole.
- Asphaltene inhibitors do not inhibit
  Asphaltene precipitation, but they disperse precipitated Asphaltenes.
- Pressure Control Pressure decreases can cause Asphaltenes to precipitate, providing pressure support can prevent this.
- Aromatic solvents (xylene soaking)
  - Frequency
  - Duration

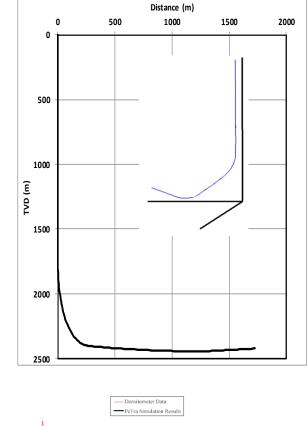
#### **Erosion and Sand**

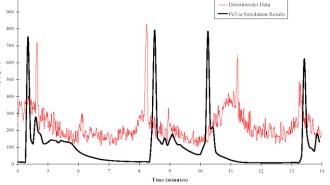
- Sand production rate is generally an input from completions and some times it is go-by number.
- Sand production and erosional limits can be determined by using
  - API 14 E
  - TULSA Model
  - CFD
- Selecting right location for sand monitoring is key.
- In the operations phase online monitoring is used to detect sand influx.
- Production rate control is used to stay within allowable limits
- Sand prone wells can be re-completed
- Water hammer could cause fines migrations
- Bullheading through gravel pack (used to displace water below SCSSV for hydrate control) may affect completion, leading to sand production



# **Transient Multiphase Flow Modeling**

- Slugging
  - Slug flow is the dominant flow regime in upward flow.
  - Complex well geometries, especially long horizontal wells.
    - Toe up
    - Toe down
  - Low flowrates
  - Changes in flow conditions
- Complex Thermal Modeling
  - Counter current flow
- Intervention Modeling
- Drilling
- Well kill
- Near wellbore flow modeling







#### **Artificial Lift and Flow Assurance**

#### • Pumps cause major changes in downhole systems

- Significant Pressure increase
  - Asphaltene Deposition
  - Scale Precipitation
- Added Heat to the system
  - ESP's generate significant heat, this can cause scale to precipitate, especially at the outer surface of the pump.
- High viscosities due to tight emulsions also adversely affect pump efficiency
- Erosion



#### **Artificial Lift and Flow Assurance**

- Gas lift can also change FA issues down hole
  - Gas lift expands hydrate formation conditions and increases risk for hydrate formation.
  - Gas lift can cause Asphaltene precipitation.
  - Gas lift injection through annulus can cause lower temperatures in the upper part of the tubing which can cause wax deposition.



# **Chemical Injection Locations**

#### **Wellhead Injection**

To support well and downstream operations

- Methanol / Glycol
- LDHI
- Scale
- Corrosion

#### SCSSV Injection

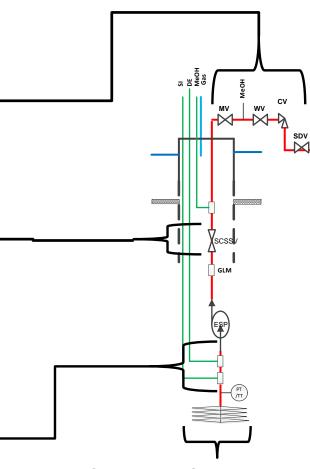
Generally for Hydrate Management

- Methanol / Glycol
- LDHI

#### **Deep Downhole Injection**

**Continuous Production treatment** 

- Scale
- Wax
- Asphaltene
- Emulsion
- Corrosion
- H<sub>2</sub>S Scavenger



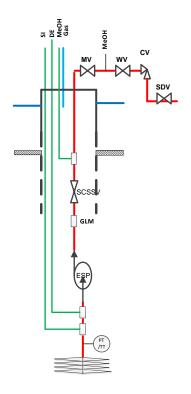
#### **Chemical Squeezes**

- Scale
- Asphaltene



# **Chemical Injection Design**

- Flow Assurance determine chemical injection
  - Location
  - Control line size
  - Rate
  - Pressure
  - Time and duration (continuous vs. intermittent)
  - Operability (cracking pressure)





# **Flow Assurance Famous Scary Pictures**





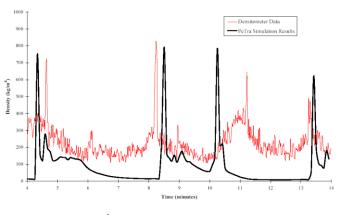
Asphaltene





Stat Oil Wax Nalco Scale

Petrobras Hydrate



Slugging





# **Flow Assurance Integration**

# Flow Assurance helps identify

- Risk
- Mitigation/Management
- Contingency
- Develop Procedures

# Flow Assurance works with interfaces

- Reservoir
- Production Engineers
- Artificial Lift
- D&C
- Surface and Subsea Facilities



# Questions ?

